



BIONICO PROJECT - PRELIMINARY ASSESSMENT OF HYDROGEN PRODUCTION FROM BIOGAS USING A FLUIDISED BED CATALYTIC MEMBRANE REACTOR M. Binotti, G. Di Marcoberardino, G. Manzolini

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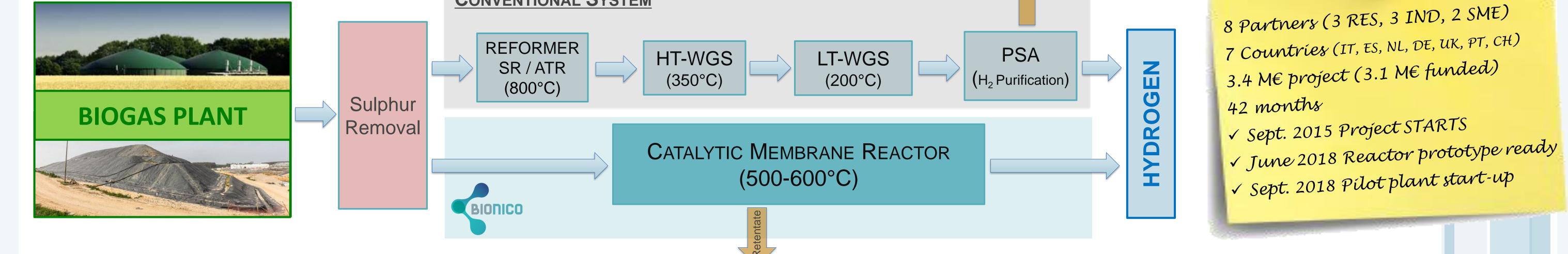
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MOTIVATION AND CONCEPT

The current challenges of energy saving and reduction of CO₂ emissions must deal with the significant growth of energy demand. Hydrogen is a promising energy carrier that can replace fossil fuels in power generation and transportation, drastically reducing local pollution and CO₂ emission. In order to have a sustainable hydrogen economy, conventional production processes based on natural gas steam reforming have to be replaced with alternative production systems relying on renewable energy sources. The BIONICO project uses biogas, obtained by anaerobic digestion of residual biomass or other waste material, as a renewable source for green hydrogen production.

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The BIONICO project will develop, build and demonstrate a novel reactor concept integrating H₂ production and separation in a single vessel in a biogas production plant. The hydrogen production capacity will be of 100 kg/day, with target purity of 99,99%. By using the novel intensified reactor, direct conversion of biogas to pure hydrogen is achieved in a single step, which results in an increase of the overall efficiency and component savings and potential cost reduction.



CONVENTIONAL SYSTEM

PRELIMINARY PERFORMANCE ASSESSMENT

Three different fuel processors and their relative balance of plant are modelled in Aspen Plus[®], where mass and energy balances are solved; all the modelled reactors (SMR, ATR, ATR-MR, HT-WGS, LT-WGS), considering the relatively high catalyst load, were assumed to achieve chemical equilibrium determined through Gibbs free energy minimization. The analysis consider that biogas flow is already exempt of sulphur content adopting a sulphur removal unit (e.g. based on active carbon) upstream the reforming system to avoid catalysts and membranes poisoning. This step is not shown in the layout being neutral to the purpose of the work and common to all the configurations. The auxiliary values adopted for the BoP result from benchmark technologies, typical O&M specifications, requirements for the materials.

LANDFILL GAS						
	units	values				
CH ₄	% mol	44.2				
CO ₂		34				
N ₂		16				
02		2.7				
CO, H ₂		trace				
H ₂ O		Saturated				
LHV	MJ/ka	12.7				

The system efficiency is determined for the three configurations:

$$\eta_{sys} = \frac{\dot{m}_{H_2} LHV_{H_2}}{\left(\dot{m}_{BG_f} + \dot{m}_{BG_{aux}}\right) LHV_{BG}} + \frac{W_{aux}}{\eta_{el,rif}}$$

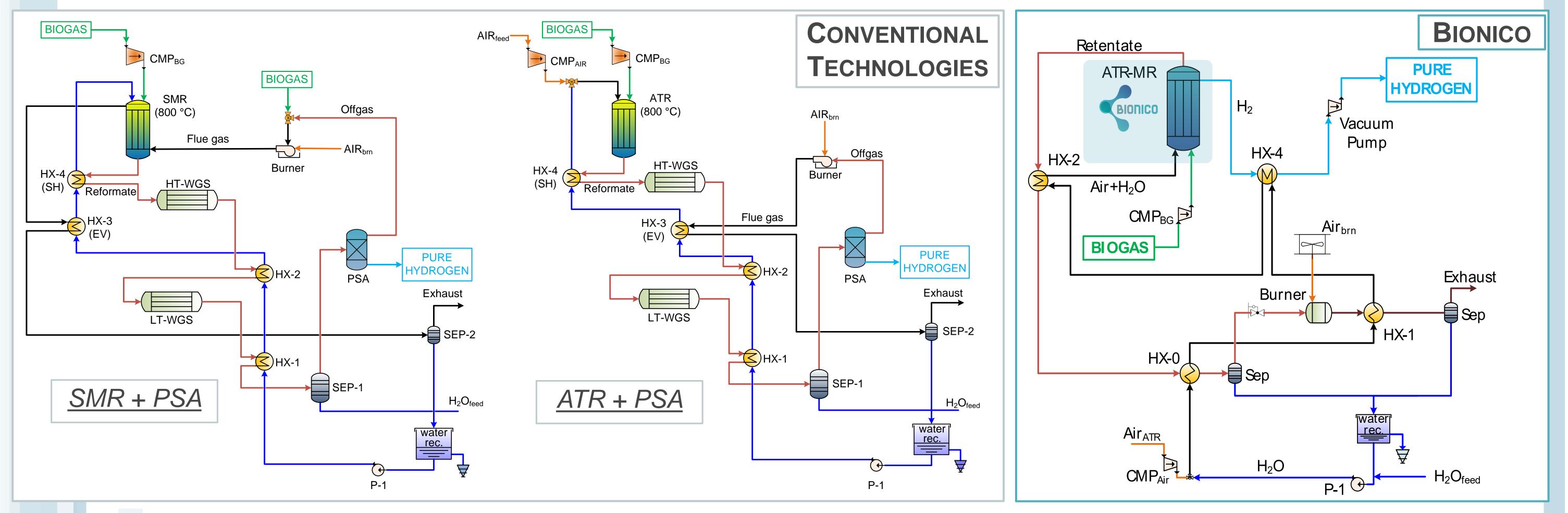
- \circ LHV_{H2} is equal to 120 MJ/kg
- W_{aux} is the sum of the electric consumptions of the system auxiliaries (i.e. compressors, pumps, control system)
- \circ $\eta_{el,rif}$ is set equal to 45%, as the average electric efficiency of the

		CONVENTIONAL		BIONICO
	units	SR	ATR	ATR-MR
Hydrogen mass flow	Kg/day	100	100	100
Max Temperature	°C	800	800	550
Pressure	bar	8-14	8-14	8-14
S/C	-	4	3	3
PSA efficiency	%	78-86	78-86	-
Aux el. efficiency	%	70	70	70









RESULTS & CONCLUSIONS

	REF. TECHNOLOGY		BIONICO	Main results show that the BIONICO system efficiency (69.2%) is about 25% and
unite	CD	ΛTD		17% higher with respect to ATR and SMR cases respectively. This record

	units	JN	AIN	
Biogas Input	Nm³/h (kW)	35.7+14.6 (221)	47.0 (207)	36.8 (162)
BG/Air compressors	kW	6.2/-	8.1/11.6	4.4/3.4
Vacuum pump + H ₂ compressor	kW	_	-	8.6
System efficiency	% _{LHV}	59.2	55.4	69.2
Membrane Area	m²	-	-	3.1

The might with respect to Arry and Own cases respectively. This record efficiency is reached at a much lower temperature with respect to SMR and ATR thanks to the use of the CMR that allows for hydrogen production and separation in a single step, moving the equilibrium of the reactions towards the products.

4TH INTERNATIONAL CONFERENCE ON RENEWABLE ENERGY GAS TECHNOLOGY, REGATEC 2017, 22-23 MAY 2017, PACENGO (VERONA), ITALY



THIS PROJECT HAS RECEIVED FUNDING FROM THE FUEL CELLS AND HYDROGEN 2 JOINT UNDERTAKING UNDER GRANT AGREEMENT NO 671459. THIS JOINT UNDERTAKING RECEIVES SUPPORT FROM THE EUROPEAN UNION'S HORIZON 2020 RESEARCH AND INNOVATION PROGRAMME HYDROGEN EUROPE AND N.ERGHY. NOTE: THE PRESENT WORK REFLECTS ONLY THE AUTHOR'S VIEWS AND THE FCH JU AND THE UNION ARE NOT LIABLE FOR ANY USE THAT MAY BE MADE OF THE INFORMATION CONTAINED THEREIN